

Mid-term 2004

1. Excavate and remove

Low volatility means SVE will not work

High K_{oc} means P&T will not work

2. s/s

Metals are generally not volatile - SVE will not work

Metals generally do not biodegrade

3. Note gasoline contains butane, pentane, benzene, toluene, and xylene, so results are mixed:

very likely success for lightest hydrocarbons (butane)
somewhat likely for BTEX, pentane

Somewhat likely overall

3 points for somewhat likely answer

2 points for recognizing nature of mixture

4. Values from Heath

Medium sand

$$K \approx 8 \text{ m/d}$$

$$i = 0.007$$

$$n = 0.25$$

$$V = \frac{Ki}{n} = 0.2 \text{ m/d} = 0.7 \text{ ft/d}$$

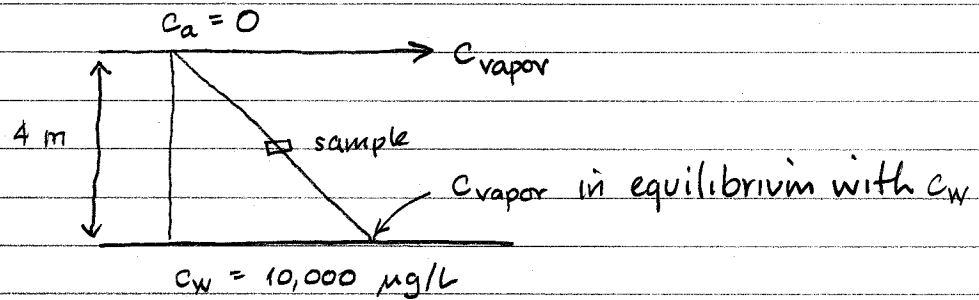
From PRB chart: Want 5000 \rightarrow 5 (1000-fold reduction)

$$W \approx 3 \text{ ft} \approx 1 \text{ m} \quad \text{for } t_{1/2} = 10$$

5. Anaerobic conditions favors biodegradation of chlorinated compounds = PCE, carbon tet and denitrification of NO_3
Benzene, toluene, and petroleum hydrocarbons need aerobic conditions to degrade, so will not be degraded

6. Methylene chloride is a common laboratory artifact - MeCl is probably not in actual ground water since it is not in site soils

7. Soil vapor conc will look like this:



c_{vapor} at g-w interface = $\frac{c_v}{c_w} = H'$

$$H = 9.1 \times 10^{-3} \frac{\text{atm m}^3}{\text{mol}}$$

$$H' = \frac{H}{RT} = \frac{9.1 \times 10^{-3} \frac{\text{atm m}^3}{\text{mol}}}{8.2 \times 10^{-5} \times 293 \frac{\text{atm m}^3}{\text{mol} \cdot \text{K}}} = 0.38$$

5 pts
to get C_G

$$C_G = 3800 \text{ mg/L}$$

Under steady-state, with zero advection, soil gas conc is given by:

5 pts to
get right
problem
structure

$$\frac{\partial C_G}{\partial t} = 0 = -v \frac{\partial C_G}{\partial z} + D \frac{\partial^2 C_G}{\partial z^2}$$

$$D \frac{\partial^2 C_G}{\partial z^2} = 0 \rightarrow \frac{\partial C_G}{\partial z} = \text{constant}$$

Linear C_G gradient as shown above

7. cont

Since sample is halfway between w.t. and g.s.,

$$C_G = \frac{1}{2} \cdot 3800 = 1900 \text{ } \mu\text{g/L}$$

Consider partitioning from gas to soil water:

$$C_W = C_G / H' \approx 5000 \text{ } \mu\text{g/L}$$

Consider partitioning from soil water to soil

$$C_S = K_d C_W$$

$$K_d = f_{oc} K_{oc} = 0.001 \cdot 126 \frac{\text{ml}}{\text{g}} = 0.126 \frac{\text{ml}}{\text{g}}$$

5 pts →
to get C_S

$$C_S = 0.126 \frac{\text{ml}}{\text{g}} \cdot 5000 \frac{\mu\text{g}}{\text{L}} \cdot \frac{1}{1000} \frac{\text{L}}{\text{ml}}$$

$$= 0.63 \text{ } \mu\text{g/g}$$

$$= 630 \text{ } \mu\text{g/kg} \approx 0.63 \text{ mg/kg}$$

5 pts. → Total conc in soil sample (from Lecture 3)
to get C_T

$$C_T = \rho_b C_S + \theta_w C_W + \theta_g C_G$$

$$= 1.65 \frac{\text{g}}{\text{cm}^3} \cdot 0.63 \frac{\text{mg}}{\text{kg}} + 0.4 \cdot 0.25 \cdot 5000 \frac{\mu\text{g}}{\text{L}}$$

$$+ 0.4 \cdot 0.75 \cdot 1900 \frac{\mu\text{g}}{\text{L}}$$

$$\text{Soil} = 1.65 \frac{\text{g}}{\text{cm}^3} \cdot 1000 \frac{\text{cm}^3}{\text{L}} \cdot 0.63 \frac{\text{mg}}{\text{kg}} \cdot \frac{1}{1000} \frac{\text{kg}}{\text{g}} \cdot 1000 \frac{\mu\text{g}}{\text{mg}}$$

7. cont

Soil	-	1040	$\frac{\mu\text{g}}{\text{L}}$
Water		500	$\frac{\mu\text{g}}{\text{L}}$
Air		570	$\frac{\mu\text{g}}{\text{L}}$
Total		2,110	$\frac{\mu\text{g}}{\text{L}}$

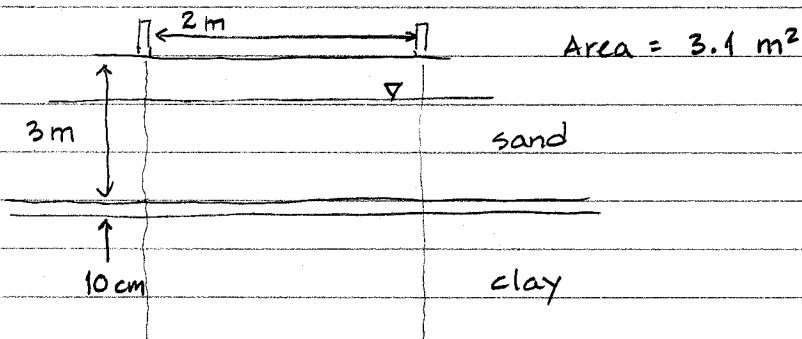
In terms of dry mass, 1 L = 1.65 Kg

$$\frac{2110 \frac{\mu\text{g}}{\text{L}}}{1.65 \frac{\text{kg}}{\text{L}}} = 1280 \frac{\mu\text{g}}{\text{kg}}$$

$$= 1.3 \frac{\text{mg}}{\text{kg}}$$

Yes ground water could contaminate soil
to 1 mg/Kg

8.



$$\text{Volume in sand column beneath spill area} = 3 \cdot 3.1 = 9.3 \text{ m}^3 = \cancel{V}$$

$$\text{Volume of voids} = 0.25 \cdot 9.3 = 2.3 \text{ m}^3 = \cancel{V}$$

$$\begin{aligned} \text{Volume for TCE residual} &= S_r \cdot \cancel{V} \\ &= 0.2 \cdot 2.3 = 0.47 \text{ m}^3 \end{aligned}$$

$$\text{TCE spill} = 1 \text{ m}^3 > S_r \cdot \cancel{V} = 0.47 \text{ m}^3$$

10 pts

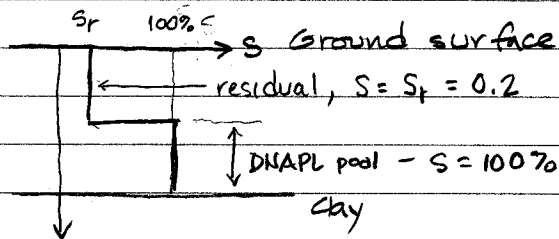
∴ TCE will reach clay layer as DNAPL

for residual

calc

Compute ponding height on clay. Assume TCE in excess of residual saturation will saturate sand above clay. Saturation profile looks like this

10 pts for recognizing this mass balance



$$\text{Mass accounting} \quad \cancel{V}_{\text{total}} = 1 \text{ m}^3 = \cancel{V}_{\text{residual}} + \cancel{V}_{\text{pool}}$$

$$= A (H_{\text{residual}} \cdot S_r \cdot n + H_{\text{pool}} \cdot n)$$

$$= A ([3 - H_{\text{pool}}] \cdot S_r \cdot n + H_{\text{pool}} \cdot n)$$

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$$V_{\text{total}} = A \cdot m \left(3 S_r + H_{\text{pool}} (1 - S_r) \right)$$

$$1 \text{ m}^3 = 3.1 \text{ m}^2 \cdot 0.25 \left(3 \text{ m} \cdot 0.2 + H_{\text{pool}} 0.8 \right)$$

Solve for height of pool:

$$H_{\text{pool}} = 0.86 \text{ m}$$

$$\text{check } 0.86 \cdot 3.1 \cdot 0.25 = 0.67 \text{ m}^3 = V_{\text{pool}}$$

$$(3 - 0.86) 3.1 \cdot 0.25 \cdot 0.2 = 0.33 \text{ m}^3 = V_{\text{res}}$$

$$\Sigma = 1 \text{ m}^3 \checkmark$$

Height of DNAPL above linear fracture

From Homework 2, height of DNAPL to achieve entry pressure is:

$$H_c = \frac{2\sigma}{\Delta\rho g D}$$

10 pts for fracture calc.

$$\sigma = 34.5 \text{ dyn/cm} = 34.5 \text{ g/cm}^2 \cdot \text{s}$$

$$\Delta\rho = 1.46 - 1.00 = 0.46 \text{ g/cm}^3$$

$$D = 20 \text{ }\mu\text{m} = 2 \times 10^{-3} \text{ cm}$$

$$H_c = \frac{2 \cdot 34.5 \text{ g/cm}^2 \cdot \text{s}}{0.46 \text{ g/cm}^3 \cdot 980 \text{ cm/s}^2 \cdot 2 \times 10^{-3} \text{ cm}}$$

$$= 76 \text{ cm} = 0.76 \text{ m}$$

The DNAPL will barely penetrate the clay

9. G-w velocity $v = \frac{K_i}{n} = \frac{0.1 \text{ cm/s} \cdot 0.0025}{0.25}$

2 pts

$$= 0.001 \text{ cm/s}$$

$$= 0.86 \text{ m/d}$$

Use 1-D transport equation from Lecture 3 =

$$c(x,t) = \frac{c_0}{2} \operatorname{erfc} \left(\frac{R_d x - ut}{\sqrt{4R_d D_H t}} \right)$$

5 pts for
correct

Assume $c_0 = \text{solubility} = 1100 \text{ mg/L}$

c_0

From chart by Gelhar et al in Lecture 3, for length scale of 200 m, $\alpha_L \approx 10 \text{ m}$

4 pts

$$D_H = \alpha_L v = 10 \text{ m} \cdot 0.86 \text{ m/d} = 8.6 \text{ m}^2/\text{d}$$

2 pts

$$K_d = K_{oc} f_{oc} = 126 \frac{\text{ml}}{\text{g}} \cdot 0.005 = 0.63 \frac{\text{ml}}{\text{g}}$$

2 pts

$$R_d = 1 + \frac{\rho_b K_d}{n} = 1 + \frac{1.6 \text{ g/ml} \cdot 0.63 \text{ ml/g}}{0.25}$$

$$= 5.0$$

5 pts

for correct
eqn and
solution

See attached spreadsheet for solution: concentration will exceed MCL within one year — Need to work faster!

n	0.25	
i	0.0025	
K	0.1 cm/s	
V	0.0010 cm/s	= $K i / n$
V	0.864 m/d	
α_L	10 m	
D_H	8.64 m ² /d	= $\alpha_L V$
f_{oc}	0.005	
K_{oc}	126 ml/g	
K_d	0.63 ml/g	= $f_{oc} K_{oc}$
ρ_b	1.6 g/ml	
R_d	5.032	= $1 + K_d \rho_b / n$
x	200 m	
t	365 d	
C_0	1100000 ug/L	
$C(x,t)$	58 ug/L	= $C_0 / 2 \operatorname{erfc} ((R_d x - V t) / \operatorname{sqrt} (4 R_d D_H t))$