

LECTURE # 11

1.060 ENGINEERING MECHANICS II

THE MOMENTUM PRINCIPLE

$$\frac{\partial}{\partial t} \int_{\mathcal{V}_0} \rho \vec{q} d\mathcal{V} = \int_{\mathcal{V}_0} \rho \vec{g} d\mathcal{V} + \sum \vec{M}P + \left\{ \begin{array}{l} \text{Sum of all} \\ \text{other forces} \\ \text{acting on fluid in } \mathcal{V}_0 \end{array} \right\}$$

$\vec{M}P$ = Thrust (Momentum, M , & Pressure P) at inflow/outflow section of \mathcal{V}_0 , A_{in} & A_{out}

If flow is well behaved at A_{in} & A_{out} :
Straight parallel streamlines $\perp A$

then

$$\vec{M}P = \left[\int_{A_f} (\rho q_{\perp}^2 + p) dA \right] (-\vec{n}_A) = \left[(K_m \rho V^2 + P_{CG}) A_f \right] (-\vec{n}_{A_f})$$

$$K_m = \int_{A_f} q_{\perp}^2 dA / (V^2 A_f) \approx 1 \quad (\text{very well behaved})$$

$$V = Q/A_f ; \quad P_{CG} = \text{pressure at Center of Gravity of } A_f$$

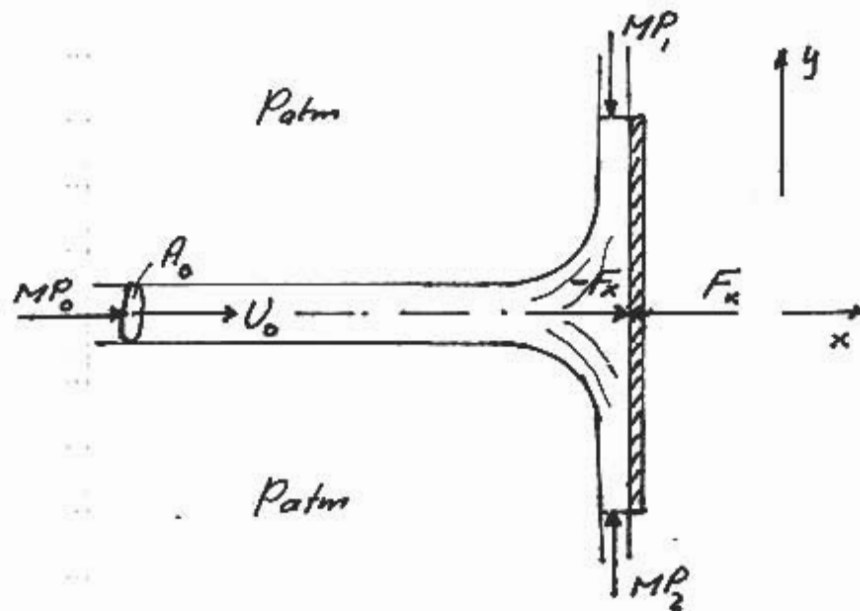
FOR STEADY FLOW : $\partial/\partial t = 0$

$$\int_{\mathcal{V}_0} \rho \vec{g} d\mathcal{V} + \sum \vec{M}P + \sum \vec{\text{all other forces on fluid in } \mathcal{V}_0} = 0$$

$|\vec{M}P| = \rho V^2 A_f + P_{CG} A_f$ and it acts INWARDS
TOWARDS \mathcal{V}_0 in direction $\perp A_f$

$$\sum \vec{\text{Forces on } \mathcal{V}_0} = - \sum \vec{\text{Forces from } \mathcal{V}_0}$$

EXAMPLE I: The Firehose



Gravity acts in $-z$.

Plate wide enough to completely deflect the jet

Jet is freely "falling"

In x-direction

$$MP_{0x} + \underbrace{MP_{1x} + MP_{2x}}_{=0} + F_x = 0$$

$$F_x = \text{force on fluid from plate} = -MP_{0x} = -p_0 A_0 - \rho U_0^2 A_0$$

0 since $p_0 = 0$

$$\underline{-F_x} = \text{force from fluid on plate} = \underline{\rho U_0^2 A_0}$$

Firehose acts as a "pressure" force $(\rho U_0^2) A_0$

In y-direction

$$MP_{0y} + MP_{1y} + MP_{2y} = 0 \Rightarrow MP_1 = MP_2$$

= 0

$p_1 = p_2 = 0$ since jets in atmosphere

$A_1 = A_2$ because of symmetry

$$(p_1 + \rho U_1^2) A_1 = (p_2 + \rho U_2^2) A_2 \Rightarrow \underline{U_1 = U_2}$$

But what is U_1 & U_2 ?

Bernoulli along surface streamlines from "0" to "1" and "0" to "2", with same z and $\rho_0 = \rho_1 =$

$\rho_2 = \rho$:

$$\frac{1}{2} \rho U_0^2 = \frac{1}{2} \rho U_1^2 \quad \text{and} \quad \frac{1}{2} \rho U_0^2 = \frac{1}{2} \rho U_2^2$$

$$\underline{U_0 = U_1 = U_2}$$

Note: If flow in xz -plane gravity enters the problem and we get from Bernoulli:

$$\rho g z_0 + \frac{1}{2} \rho U_0^2 = \rho g z_1 + \frac{1}{2} \rho U_1^2 = \rho g z_2 + \frac{1}{2} \rho U_2^2$$

or

$$U_1^2 = U_0^2 + 2g(z_0 - z_1) ; \quad U_2^2 = U_0^2 + 2g(z_0 - z_2)$$

Thus,

$$U_0 \approx U_1 \approx U_2$$

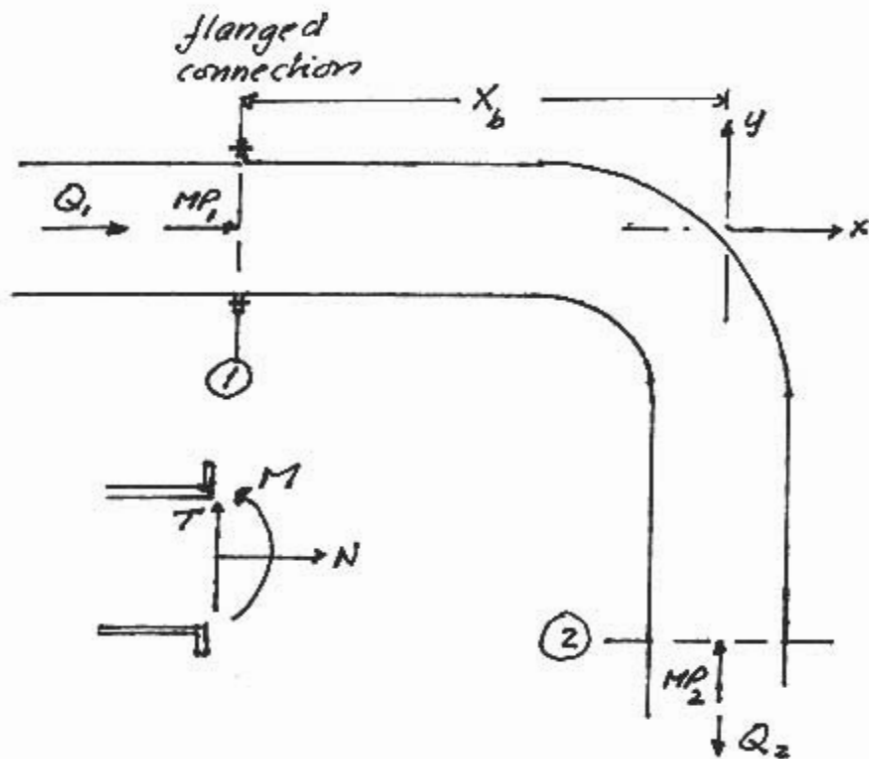
still hold if

$$\underline{\frac{U_0^2}{2g} = \text{velocity head} \gg \begin{cases} |z_0 - z_1| \\ |z_0 - z_2| \end{cases} = \text{elevation difference}}$$

In problem where the characteristic velocity head, $V^2/2g$, is much larger than elevation differences, these may be neglected.

In momentum principle applications this translates into a neglect of gravity forces is acceptable when $V^2/2g \gg \Delta z$.

EXAMPLE II: Flow around a bend



Gravity acts in z . (Neglect here)
 Find forces & moment (in xy -plane) on flange at 1-1

Flow well behaved at 1-1 & 2-2 (far enough from bend)

Volume Conservation (always!)

$$Q_1 = Q_2 = Q ; A_1 = A_2 = A \Rightarrow V_1 = \frac{Q}{A_1} = V_2 = \frac{Q}{A_2} = V$$

Momentum in x-direction

$$MP_1 + F_x = 0 \Rightarrow F_x = -MP_1 = -(\rho V^2 + p_{CG,1}) A$$

$$\text{Force on Pipe} = -\text{Force on Fluid} = -F_x = (\rho V^2 + p_{CG,1}) A = N$$

Momentum in y-direction

$$MP_2 + F_y = 0 \Rightarrow F_y = -MP_2 = -(\rho V^2 + p_{CG,2}) A$$

$$\text{Force on pipe} = -F_y = (\rho V^2 + p_{CG,2}) A = T$$

Moment of forces around flanged connection

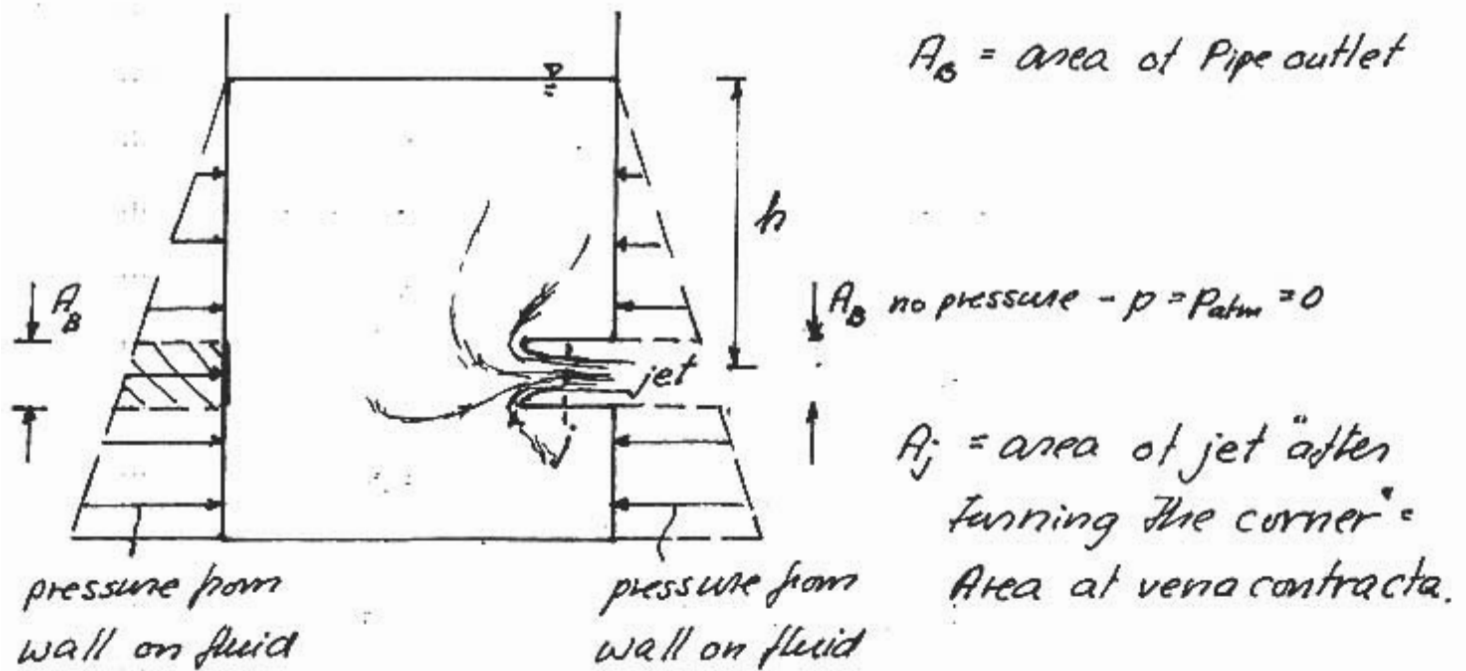
MP is acting as a total force - so just use it as such to get moments around CG at 1-1.

MP_1 has no moment arm $\Rightarrow MP_1$ has no contribution

MP_2 has moment arm = x_b , so

$$\underline{M} = MP_2 \cdot x_b = (\rho V^2 + p_{CG,2}) A x_b \quad (\text{counter clockwise})$$

EXAMPLE III: Borda's Mouthpiece



Bernoulli

$$\rho g h = \frac{1}{2} \rho V_j^2 \Rightarrow \underline{V_j^2 = 2 g h}$$

Momentum

Unbalanced pressure force from wall area A_B opposite Borda's mouthpiece = $\rho g h A_B$ = Momentum force ($p_j = 0$ since jet is free) at vena contracta = $\rho V_j^2 A_j$. Or $\underline{V_j^2 = g h (A_B / A_j)}$

Bernoulli & Momentum

Same V_j requires that

$$\underline{A_j / A_B = \text{Contraction Coefficient} = 0.5}$$

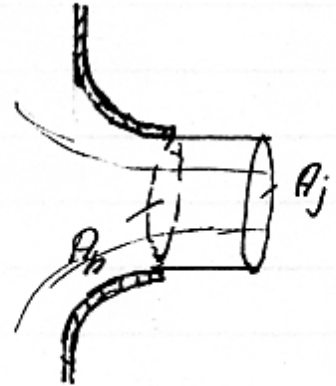
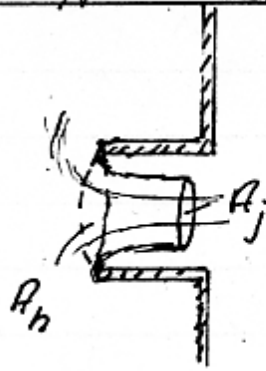
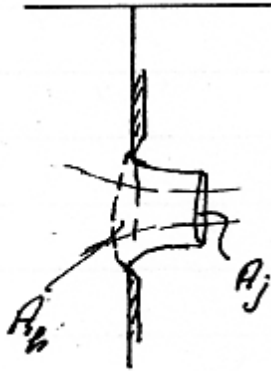
for Borda's Mouthpiece

Reason why this works here

Basic assumption is hydrostatic pressure along container walls everywhere, i.e. small velocities at walls. This holds here since $V \approx 0$ at the corner where pipe penetrates the container walls. Not so if orifice is in wall itself since $V \neq 0$ near hole.

GENERAL OUTFLOW CONDITIONS

Contraction Coefficients



$$C_v = A_j / A_h \approx 0.6$$

$$C_v = 0.5$$

$$C_v = 1.0$$

Note: Contraction Coefficient refers to the ratio of AREAS of jet at vena contracta and orifice, not the diameter ratio (if circular orifice). For a 2-D orifice, i.e. a slot, Area = height \cdot length and $C_v = (h_j \cdot l_j) / (h_h \cdot l_h) \approx h_j / h_h$ since $l_j \approx l_h$ if $l_h \gg h_h$. Looks like a "length" ratio, but it is really an "area per unit length" ratio.

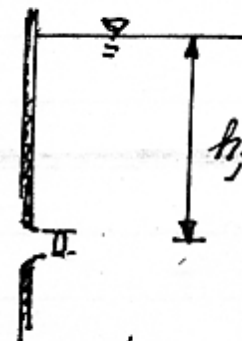
Outflow Pressure Conditions

Free Outflow

Submerged Outflow



$$P_j = P_{atm} = 0$$



$$P_j = \rho g h_j$$

Generalized

Pressure at CG of jet at vena contracta = pressure in receiving body of fluid at that elevation.